

$Nu \sim Ra^{1/2}$ scaling enabled by multiscale wall roughness in Rayleigh–Bénard turbulence

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In turbulent Rayleigh-Bénard (RB) convection with regular, mono-scale, surface roughness, the scaling exponent β in the relationship between the Nusselt number Nu and the Rayleigh number Ra, $Nu \sim Ra^{\beta}$ can be $\approx 1/2$ locally, provided that Ra is large enough to ensure that the thermal boundary layer thickness λ_{θ} is comparable to the roughness height. However, at even larger Ra, λ_{θ} becomes thin enough to follow the irregular surface and β saturates back to the value for smooth walls (Zhu *et al.*, Phys. Rev. Lett., vol. 119, 2017, 154501). In this paper, we prevent this saturation by employing multiscale roughness. We perform direct numerical simulations of two-dimensional RB convection using an immersed boundary method to capture the rough plates. We find that, for rough boundaries that contain three distinct length scales, a scaling exponent of $\beta = 0.49 \pm 0.02$ can be sustained for at least three decades of Ra. The physical reason is that the threshold Ra at which the scaling exponent β saturates back to the smooth wall value is pushed to larger Ra, when the smaller roughness elements fully protrude through the thermal boundary layer. The multiscale roughness employed here may better resemble the irregular surfaces that are encountered in geophysical flows and in some industrial applications.

Key words: Bénard convection, turbulent convection

1. Introduction

Rayleigh-Bénard (RB) convection (Ahlers, Grossmann & Lohse 2009; Lohse & Xia 2010; Chillà & Schumacher 2012; Xia 2013), a flow in a container heated

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from below and cooled from above, is a paradigmatic system in thermally driven turbulence. The key control parameters are the Rayleigh number and Prandtl number, which are respectively defined as $Ra = \alpha g \Delta L^3 / (\nu \kappa)$ and $Pr = \nu / \kappa$, where α is the thermal expansion coefficient, g the gravitational acceleration, Δ the temperature drop across the container, L the height of the fluid domain, ν the kinematic viscosity, and κ the thermal diffusivity of the fluid. The most relevant response of the system is the heat transfer, which in dimensionless form is expressed as the Nusselt number Nu.

Over the years, much attention has been paid to the scaling relation between Nu and Ra, i.e. $Nu \sim Ra^{\beta}$. Two of the early attempts were made by Malkus (1954) and Priestley (1954), both of whom independently proposed $\beta = 1/3$, which reflects their assumption that the heat flux is independent of the distance between the two plates and controlled only by the boundary layers (BLs). Grossmann & Lohse (2000, 2001), based on an analysis and decomposition of the kinetic and thermal energy dissipation rates into bulk and BL contributions, proposed that there are no pure scaling laws but rather a superposition of various ones. For extremely large Ra, Kraichnan (1962) predicted a so-called ultimate regime with turbulent shear BLs, which led to the relation $Nu \sim Ra^{1/2} (\ln Ra)^{-3/2}$, where the logarithmic correction becomes negligible with increasing Ra (Spiegel 1963). Yet there are still debates on the various claims of evidence for this regime. With a low-temperature helium RB experiment, Chavanne et al. (1997, 2001) found that β increases to 0.38 for $Ra = (2 \times 10^{11}, 10^{14})$. Taking into account the effects of turbulent BLs, Grossmann & Lohse (2011) derived a scaling law with a different logarithmic correction as compared to Kraichnan (1962) and formulated this relation as an effective power law with a locally determined effective scaling exponent β . In particular, they derived that β should be approximately 0.38 when Ra is approximately 10¹⁴. This was demonstrated experimentally by He *et al.* (2012*a*,*b*). For more information on general aspects of RB convection, we refer the readers to the reviews by Ahlers et al. (2009), Lohse & Xia (2010), Chillà & Schumacher (2012) and Xia (2013).

To avoid the influence of the BLs, and therefore to avoid the logarithmic corrections, several successful model systems have been proposed throughout the years. In numerical experiments with periodic boundary conditions in all directions, Lohse & Toschi (2003) and Calzavarini *et al.* (2005) proposed 'homogeneous' RB turbulence; Gibert *et al.* (2006) and Pawar & Arakeri (2018) performed corresponding RB experiments in a 'cavity'; Lepot, Aumaître & Gallet (2018) proposed radiative heating convection, in which heat is input directly inside an absorption layer. When this absorption length is thicker than the BLs, radiative heating is allowed to bypass the BLs and heat up the bulk turbulent flow directly. In all these cases a scaling exponent of 1/2 was achieved, because the BLs no longer played a role. We call this regime the 'asymptotic ultimate regime'.

For conventional RB convection, in which BLs close to the bottom and top plate are formed, wall roughness has been introduced in an attempt to trigger an earlier onset of a turbulent BL; see the reviews Ahlers *et al.* (2009), Chillà & Schumacher (2012) and Xia (2013) for detailed discussions. The results for three-dimensional (3-D) simulations and experiments can be divided into two main categories. First, there are studies which show that roughness can increase the scaling exponent β from a value slightly below 1/3 to a value between 1/3 and 1/2 (Roche *et al.* 2001; Qiu, Xia & Tong 2005; Stringano & Verzicco 2006; Tisserand *et al.* 2011; Salort *et al.* 2014; Wei *et al.* 2014; Xie & Xia 2017). Shen, Tong & Xia (1996), Du & Tong (2000), Wei *et al.* (2014) and Xie & Xia (2017) found that the scaling exponent β remains roughly the same when roughness is introduced. Whether an increase in the scaling

exponent is observed or not depends on the roughness configuration and the explored Ra and Pr regime. Roche et al. (2001) designed the first experiment to possibly reach the ultimate regime without the logarithmic correction (asymptotic ultimate regime) using a cylindrical cell with grooved roughness in both plates and in the sidewall. They observed a scaling exponent β of 0.51 in the Rayleigh number range $Ra = (2 \times 10^{12}, 5 \times 10^{13})$. Wagner & Shishkina (2015) showed in direct numerical simulations (DNS) for rectangular roughness that the scaling exponent β increases compared to the smooth case for low Ra before it saturates back to the smooth wall value at large Ra. For RB with pyramid-shaped roughness, Xie & Xia (2017) varied the roughness aspect ratio λ , which they define as the height of a roughness element over its base width, from 0.5 to 4.0. With increasing *Ra* they identified three regimes. The transition between regime I and II occurs when the thermal BL becomes thinner than the roughness height and the transition between regime II and III occurs when the viscous BL thickness becomes smaller than the roughness height. They found that in regime II the scaling exponent β increases from 0.36 to 0.59 when λ is increased from 0.5 to 4.0. In regime III they found that these scaling exponents saturate to 0.30 to 0.50, respectively, with increasing λ . Rusaouën *et al.* (2018) performed RB experiments with water in cylindrical containers for Ra up to 10^{12} . They performed a set of measurements using smooth and rough plates with cubic roughness elements in a square lattice. In these experiments several regimes were identified for the rough case. With increasing Ra they first observed a regime in which the heat transfer is similar to the smooth case, followed by a regime in which the heat transfer is enhanced by a modification of the Nu versus Ra number scaling, before a third regime is obtained in which the heat transfer scaling is similar to the smooth case. but with a larger prefactor.

For all the rough wall RB studies that we mentioned above, a 3-D geometry of the cell has been adopted. Recently, using DNS of two-dimensional (2-D) RB convection with roughness of varying heights and wavelengths for Pr = 1, Toppaladoddi, Succi & Wettlaufer (2017) observed the existence of $\beta = 0.483$ by fitting the data in the range $Ra = (4.6 \times 10^6, 3 \times 10^9)$ and interpreted this exponent as an achievement of the ultimate regime. In contrast, Zhu *et al.* (2017) showed that: (i) there is no pure scaling exponent in that *Ra* range; (ii) although β can locally reach 1/2 in the range $Ra = (10^8, 3 \times 10^9)$, this should not be interpreted as the attainment of the ultimate regime, because a further increase of Ra leads to another regime where a thin thermal BL uniformly follows the rough surfaces, and thus the classical BL-controlled regime is recovered, causing the scaling to saturate to the classical effective *Nu* versus *Ra* scaling exponent close to 1/3.

The main question we want to address in this paper is: can the range of Ra where the effective 1/2 scaling exponent manifests be extended? We note that in all the studies mentioned above, uniform roughness of a single length scale was adopted. For this situation, the 1/2 effective exponent can be observed when roughness starts to perturb the thermal BL, as mentioned before. If, with increasing Ra, smaller and smaller roughness length scales are introduced, the different size roughness elements will protrude through the thermal BL one by one. Therefore, the flow can be maintained in a transition state and the 1/2 effective exponent can be sustained. In this manuscript, we will demonstrate this conjecture by means of multiscale wall roughness. In fact, two decades ago Villermaux (1998) theoretically pioneered the research of RB convection with multiscale cubic roughness, with power-law-distributed asperity heights. He formulated a new scaling relation and found that the heat transfer scaling exponent can be significantly enhanced. Later, Ciliberto & Laroche (1999) experimentally explored multiscale roughness by gluing glass spheres of controlled diameter on the bottom copper plate, and found that β increases to 0.45. In contrast, for a periodic roughness case, they found that the scaling exponent is similar to that in the smooth case.

Another motivation for this study is that for real-world applications and geophysical flows, the situation is far more complex, with surface roughness often containing different length scales. For example, in cities, there is huge difference among the heights of the buildings, and also natural terrains contain multiscale structure. Assuming roughness is multiscale provides a practically useful simplification (Rodriguez-Iturbe *et al.* 1994).

The paper is organized as follows: in § 2 we describe the numerical method and the parameter set-up used in the simulations. In § 3 we show how multiscale roughness alters RB turbulence. In § 4 we briefly summarize the results and give an outlook to potential future work.

2. Numerical details

We solve the Boussinesq equations with the second-order staggered finite-difference code AFiD (Verzicco & Orlandi 1996; van der Poel *et al.* 2015; Zhu *et al.* 2018*b*) in 2-D. The reason why we resorted to 2-D simulations is that they are much less expensive than the 3-D case and thus we can cover a much wider range of *Ra*. The details of the numerical methods, the parallelization and the different versions (CPU and GPU) can be found in Verzicco & Orlandi (1996), van der Poel *et al.* (2015) and Zhu *et al.* (2018*b*). The code has been extensively validated and used under various conditions (Zhu *et al.* 2017, 2018*a*,*b*). The governing equations in the dimensionless form read:

$$\frac{\partial \boldsymbol{u}}{\partial t} + \boldsymbol{u} \cdot \boldsymbol{\nabla} \boldsymbol{u} = -\boldsymbol{\nabla} p + \sqrt{\frac{Pr}{Ra}} \boldsymbol{\nabla}^2 \boldsymbol{u} + \theta \hat{\boldsymbol{z}}, \qquad (2.1)$$

$$\nabla \cdot \boldsymbol{u} = 0, \tag{2.2}$$

$$\frac{\partial\theta}{\partial t} + \boldsymbol{u} \cdot \boldsymbol{\nabla}\theta = \frac{1}{\sqrt{RaPr}} \boldsymbol{\nabla}^2\theta, \qquad (2.3)$$

where \hat{z} is the unit vector pointing in the direction opposite to gravity, \boldsymbol{u} the velocity vector normalized by the free-fall velocity $\sqrt{g\alpha\Delta L}$, t the dimensionless time normalized by $\sqrt{L/(g\alpha\Delta)}$, θ the temperature normalized by Δ , and p the pressure normalized by $g\alpha\Delta/L$. As shown in the above equations, the control parameters of the system are Ra and Pr. The boundary conditions on the top and bottom plates are no-slip for the velocity and constant for the temperature. Periodic conditions are applied to the horizontal boundaries. In all our simulations, Pr is fixed to 1. The aspect ratio is chosen as $\Gamma \equiv W/L = 2$, where W is the width of the computational domain.

For the rough cases, the characteristic length scale that we use to express Ra is the equivalent smooth wall height L'. This height is defined by determining the height of a domain with smooth boundaries that would have the same fluid volume. Nu is calculated from $Nu = \sqrt{RaPr} \langle u_z \theta \rangle_A - \langle \partial_z \theta \rangle_A$, where u_z denotes the instantaneous vertical velocity and $\langle \cdot \rangle_A$ the average over any horizontal plane between the rough plates.

An immersed boundary method (IBM) has been implemented to cope with rough surfaces (Fadlun *et al.* 2000). The basic idea of the IBM is that a body force term



FIGURE 1. (a) A sketch of the computational domain and the roughness elements. (b) Roughness element R_1 is the base element and the length scale is $R_1 = 0.1$. The structure is multiscale as $R_{n+1} = 2^{-n}R_n$, n = 1, 2, 3.

in the Navier–Stokes equation can mimic the effects of the boundaries. For more information on IBM, we refer to the reviews by Peskin (2002) and Mittal & Iaccarino (2005).

We now describe the multiscale roughness pattern: we choose a series of wall-mounted sinusoidal elements distributed on both the top and bottom plates. The sinusoidal elements all have the same aspect ratio 1. The multiscale roughness implementation is similar to that in Yang & Meneveau (2017), although in that study square roughness elements were adopted and positioned randomly. The size of the largest roughness element is used as the reference scale, $R_1 = 0.1$. At the second and third generation, we have the rough elements size as $R_{n+1} = 2^{-n}R_n$. No roughness elements of intermediate sizes are included, and the roughness height spectrum is thus discrete (Yang & Meneveau 2017). Figure 1 gives an overview of the computational domain and the roughness elements. Adequate resolution was ensured for all cases, i.e. the mesh is stretched in the wall normal direction with the finest grid implemented around the tips of the biggest roughness elements. There are at least 12 points inside the BL. The statistics were averaged over 200 free-fall time units. In the rough case for $Ra = 10^{11}$, 10240×5120 grid points, in the horizontal and vertical direction, respectively, were used. Further details about the simulation parameters can be found in appendix A.

3. Results

We first compare the flow structures for increasing Ra. Figure 2 shows the instantaneous temperature snapshots for four Ra, ranging from 10^8 to 10^{11} . At the lowest $Ra = 10^8$, within the cavity regions, the flow is viscosity dominated. Interestingly, figure 3 shows that the heat transfer for the case with multiscale roughness is approximately 15% lower than for the case with smooth walls. The same phenomenon of heat transfer reduction due to roughness was observed by Shishkina & Wagner (2011) and Zhang *et al.* (2018). The physical reason for the heat transfer reduction is that the hot/cold fluid is trapped between the roughness elements, which thus leads to a thicker thermal BL and therefore to a lower overall heat transport. For larger Ra, plumes start to develop from the tips of the roughness elements and eventually, at the largest $Ra = 10^{11}$, plumes are formed even in the sloping surfaces of the smallest rough elements. This observation indicates the impact of multiscale roughness on the flow structure and heat transfer for increasing Ra.



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FIGURE 2. The instantaneous temperature fields at (a) $Ra = 10^8$, (b) $Ra = 10^9$, (c) $Ra = 10^{10}$ and (d) $Ra = 10^{11}$. It can be seen that with Ra increasing, plumes are ejected also from smaller and smaller roughness elements.

0.5

1.0

1.5

20

Next, we check how the scaling relation evolves with increasing Ra, comparing the smooth and the multiscale case. Figure 3 shows the Nu scaling behaviour as a function of Ra, in a log-log plot and in a compensated plot. As was shown before

0.2

0



FIGURE 3. (a) Nu as a function Ra for the smooth case and the multiscale rough case. For the smooth case, the scaling exponent is $\beta = 0.29 \pm 0.01$. For the multiscale rough case, the scaling exponent is $\beta = 0.49 \pm 0.02$. As a reference, the results for mono-scale roughness are also included (Zhu *et al.* 2017), which clearly show two scaling regimes. Note that Ra is defined based on the equivalent smooth wall height. In the mono-scale roughness case, 20 sinusoidal roughness elements of the same height (0.1) were adopted. For the multiscale roughness cases considered here, 10 of these large roughness elements are replaced by one R_2 and two R_3 generation roughness geometry is 40. Nu is smaller for the multiscale roughness case than for the mono-scale roughness case, because the latter has larger roughness elements. (b) Same as in (a) but in a compensated way for the multiscale rough case. Note that we use only one specific aspect ratio for the roughness elements. If the aspect ratio changes, the scaling exponent will also change.

in 2-D RB (DeLuca *et al.* 1990; Johnston & Doering 2009; Zhu *et al.* 2017), the smooth case has an effective scaling exponent $\beta = 0.29 \pm 0.01$, extending over four decades, from $Ra = 10^8$ to $Ra = 10^{12}$. For the mono-scale roughness case, two distinct effective scaling exponent can be observed, i.e. $\beta = 0.50 \pm 0.02$, for one and half decade; then β saturates back to 0.33. With the introduction of multiscale roughness, the heat transfer is greatly enhanced. Within 95% of the confidence bound, we get the fit of $Nu \sim 0.00257Ra^{0.49\pm0.02}$ for three decades of Ra, from $Ra = 10^8$ to $Ra = 10^{11}$. A root mean square error 2.89 is found for the fit. To our knowledge, this is the first realization of such a large scaling exponent in such a wide range of Ra in RB. It is remarkable that it is realized in spite of the relatively low Ra numbers of the simulations. Obviously, as for the smooth RB, an asymptotic 1/2 exponent is expected only when Ra approaches infinity.

We will now explain the physical mechanism which leads to this considerable enhancement of the exponent for a wide range of Ra. Let us first recall why in the case of periodic roughness with one single height, the regime with an effective scaling exponent close to 1/2 survives for a limited range of Ra and then saturates back to a value close to the smooth case. In the former regime, the roughness elements start to protrude into the thermal BL. Only weak secondary vortices are generated in the cavities and the resulting mixing is not efficient. Therefore, the flow there is still dominated by viscosity. In the latter regime, secondary vortices are strong enough to mix all the fluids inside the cavities. Thus the roughness elements are covered by a thin thermal BL which is uniformly distributed along the rough surfaces, effectively

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FIGURE 4. Sketches on why regular periodic roughness with the same height leads to scaling saturation and why multiscale roughness increases the exponent in a wider range of Ra. Orange parts are the regions where the thermal BL are. (a) At lower Ra, the roughness is below the thermal BL and has little impact on scaling relations. (b,c) At intermediate Ra, the roughness starts to protrude through the thermal BL, but not to the valley of the roughness elements. For multiscale roughness, it is easy to imagine that the range of Ra is wider in this stage, as only with increasing Ra will the smaller and smaller roughness elements protrude through the thermal BL. (d) When Ra is large enough, a thin thermal BL is uniformly distributed along the rough surfaces and the scaling exponent will saturate back to the value close to the smooth case. This case is not reached in this study.

mimicking an increased wet surface area. Therefore, the effect of BL is restored and the classical BL-controlled regime is retrieved (Zhu *et al.* 2017).

Multiscale roughness essentially extends this effective 1/2 scaling regime further. Figure 4 shows sketches of thermal BLs for increasing *Ra*. As *Ra* increases, the thermal BL becomes thinner, the smaller roughness elements start to perturb the thermal BL, and this process continues until the smallest roughness elements perturb the thermal BL. Therefore, the system stays in the transitioning state and the 1/2 exponent is observed over a wider range of *Ra*, compared to the case of periodic roughness with the same height. To give further evidence for this explanation, in figure 5, we show the averaged mean temperature profiles for the valley points in the cavity regions of the roughness elements close to the wall. From the temperature profile for $Ra = 10^8$ we can detect the influence of the largest roughness R_1 . At $Ra = 10^9$ also the effect of the R_2 roughness can be identified. Last, but not least, at $Ra = 10^{10}$, the influence of smallest R_3 roughness starts to manifest.

4. Summary, discussion, and outlook

In this manuscript, we use 2-D DNS to study the effects of multiscale roughness on RB turbulence. In our case, the multiscale roughness is composed of three different roughness length scales of sinusoidal shapes. We show that with this implementation the *Nu* versus *Ra* scaling relation $Nu \sim Ra^{0.49\pm0.02}$ can be observed for at least three decades of *Ra*, while for mono-scale roughness the scaling could be observed only for only one and half decades in *Ra* (Zhu *et al.* 2017). However, there are still several open issues, for example:



FIGURE 5. Mean temperature profile as a function of the wall normal coordinate averaged at the *x*-locations of the valley points in the cavity regions, i.e. the locations where no roughness is added on top of the plate. As explained in the caption of figure 1 there are 40 roughness elements, and these profiles are averaged over all 40 corresponding valley locations.

- (i) We stress that even though we found $Nu \sim Ra^{0.5}$ over an extended Ra range, this is probably still a transitional regime and not the (asymptotic) ultimate regime in which the BLs are fully turbulent. This means that it is very likely that for the considered roughness geometry the heat transfer scaling exponent saturates back to the value of the smooth case for larger Ra. The situation may also change once the BL become turbulent. Recently, MacDonald *et al.* (2019) found an effective exponent of $\beta \approx 0.42$ in the large-Ra regime for forced convection in channel flow under the assumption that the BL profile become logarithmic.
- (ii) In this work, we modelled three different roughness length scales. We expect that with more length scales, the Ra range in which the 1/2 scaling exponent manifests might be more extended. Simulations for RB with more roughness length scales are needed to settle this question.
- (iii) The current simulations are for 2-D only and it would be interesting to see results in a fully 3-D case. Such simulations would be much more computationally intensive, but very interesting comparisons to the experimental results by, for example, Roche *et al.* (2001) would be possible. In that study a scaling exponent of approximately 1/2 up to approximately $Ra = 5 \times 10^{13}$ was observed.
- (iv) Ciliberto & Laroche (1999) observed $\beta \approx 0.45$ for RB with multiscale glass spheres glued on a copper plate. Understanding the effect of the different heat conductivities for the two roughness elements (glue and glass, both with smaller heat conductivity than copper) will be very helpful.
- (v) Here we consider only the situation for Pr = 1. Recent experiments by Xie & Xia (2017) suggest that also the Pr number might play an important role on the effect of roughness on the overall heat transport. Simulations to investigate this effect would be very interesting.
- (vi) Finally we note that for turbulent Taylor–Couette flow with mono-scale roughness that aligns in the azimuthal direction, simulations (Zhu *et al.* 2016) yielded an intermediate regime where 'Nusselt number' $Nu_{\omega} \sim Ta^{0.5}$ (angular velocity transport versus Taylor number). When *Ta* is large enough, the exponent saturates

Ra	$N_x \times N_z$	Nu
10 ⁸	2048×1024	20.8
2.15×10^{8}	2048×1024	30.1
4.64×10^{8}	3072×1536	43.6
10 ⁹	3072×1536	63.1
2.15×10^{9}	4096×2048	92.2
4.64×10^{9}	4096×2048	130.3
1010	5120×2560	189.2
2.15×10^{10}	6144×3122	273.0
4.64×10^{10}	8172×4096	390.5
1011	10240×5120	580.7

TABLE 1. *Ra*, resolution in the horizontal (n_x) and wall normal (n_z) directions, and *Nu* number for the multiscale roughness cases considered in this study. For all cases the domain aspect ratio is 2 and Pr = 1. The uncertainties in *Nu* is smaller than 1% for all cases. Corresponding information for the mono-scale roughness cases has been reported in Zhu *et al.* (2017) and for the smooth case in Zhu *et al.* (2018*a*).

back to the smooth case value. The question is whether the *Ta* range where the 1/2 exponent shows up can also be extended with multiscale roughness. For turbulent Taylor–Couette flow with mono-scale roughness that aligns in the axial direction, the asymptotic ultimate regime 1/2 scaling has already been achieved (Cadot *et al.* 1997; van den Berg *et al.* 2003; Zhu *et al.* 2018*c*), and pressure drag has been identified as the origin thereof (Zhu *et al.* 2018*c*).

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Appendix. Numerical details

The numerical details are given in table 1.

References

AHLERS, G., GROSSMANN, S. & LOHSE, D. 2009 Heat transfer and large scale dynamics in turbulent Rayleigh–Bénard convection. *Rev. Mod. Phys.* **81**, 503–538.

VAN DEN BERG, T. H., DOERING, C. R., LOHSE, D. & LATHROP, D. 2003 Smooth and rough boundaries in turbulent Taylor-Couette flow. *Phys. Rev.* E **68**, 036307.

- CADOT, O., COUDER, Y., DAERR, A., DOUADY, S. & TSINOBER, A. 1997 Energy injection in closed turbulent flows: stirring through boundary layers versus inertial stirring. *Phys. Rev.* E 56, 427–433.
- CALZAVARINI, E., LOHSE, D., TOSCHI, F. & TRIPICCIONE, R. 2005 Rayleigh and Prandtl number scaling in the bulk of Rayleigh–Bénard turbulence. *Phys. Fluids* **17**, 055107.
- CHAVANNE, X., CHILLA, F., CASTAING, B., HEBRAL, B., CHABAUD, B. & CHAUSSY, J. 1997 Observation of the ultimate regime in Rayleigh–Bénard convection. *Phys. Rev. Lett.* **79**, 3648–3651.
- CHAVANNE, X., CHILLA, F., CHABAUD, B., CASTAING, B. & HEBRAL, B. 2001 Turbulent Rayleigh-Bénard convection in gaseous and liquid He. *Phys. Fluids* 13, 1300–1320.
- CHILLÀ, F. & SCHUMACHER, J. 2012 New perspectives in turbulent Rayleigh–Bénard convection. *Eur. Phys. J.* E 35, 58.
- CILIBERTO, S. & LAROCHE, C. 1999 Random roughness of boundary increases the turbulent convection scaling exponent. *Phys. Rev. Lett.* 82, 3998–4001.
- DELUCA, E. E., WERNE, J., ROSNER, R. & CATTANEO, F. 1990 Numerical simulations of soft and hard turbulence: preliminary results for two-dimensional convection. *Phys. Rev. Lett.* 64 (20), 2370.
- DU, Y. B. & TONG, P. 2000 Turbulent thermal convection in a cell with ordered rough boundaries. J. Fluid Mech. 407, 57–84.
- FADLUN, E. A., VERZICCO, R., ORLANDI, P. & MOHD-YUSOF, J. 2000 Combined immersedboundary finite-difference methods for three-dimensional complex flow simulations. J. Comput. Phys. 161, 35–60.
- GIBERT, M., PABIOU, H., CHILLA, F. & CASTAING, B. 2006 High-Rayleigh-number convection in a vertical channel. *Phys. Rev. Lett.* **96**, 084501.
- GROSSMANN, S. & LOHSE, D. 2000 Scaling in thermal convection: a unifying view. J. Fluid. Mech. 407, 27–56.
- GROSSMANN, S. & LOHSE, D. 2001 Thermal convection for large Prandtl number. *Phys. Rev. Lett.* **86**, 3316–3319.
- GROSSMANN, S. & LOHSE, D. 2011 Multiple scaling in the ultimate regime of thermal convection. *Phys. Fluids* 23, 045108.
- HE, X., FUNFSCHILLING, D., BODENSCHATZ, E. & AHLERS, G. 2012*a* Heat transport by turbulent Rayleigh–Bénard convection for Pr = 0.8 and $4 \times 10^{11} < Ra < 2 \times 10^{14}$: ultimate-state transition for aspect ratio $\Gamma = 1.00$. New J. Phys. 14, 063030.
- HE, X., FUNFSCHILLING, D., NOBACH, H., BODENSCHATZ, E. & AHLERS, G. 2012b Transition to the ultimate state of turbulent Rayleigh–Bénard convection. *Phys. Rev. Lett.* **108**, 024502.
- JOHNSTON, H. & DOERING, C. R. 2009 Comparison of turbulent thermal convection between conditions of constant temperature and constant flux. *Phys. Rev. Lett.* **102**, 064501.
- KRAICHNAN, R. H. 1962 Turbulent thermal convection at arbitrary Prandtl number. Phys. Fluids 5, 1374–1389.
- LEPOT, S., AUMAÎTRE, S. & GALLET, B. 2018 Radiative heating achieves the ultimate regime of thermal convection. Proc. Natl Acad. Sci. USA 115 (36), 8937–8941.
- LOHSE, D. & TOSCHI, F. 2003 The ultimate state of thermal convection. Phys. Rev. Lett. 90, 034502.
- LOHSE, D. & XIA, K.-Q. 2010 Small-scale properties of turbulent Rayleigh–Bénard convection. Annu. Rev. Fluid Mech. 42, 335–364.
- MACDONALD, M., HUTCHINS, N., LOHSE, D. & CHUNG, D. 2019 Heat transfer in fully-rough-wallbounded turbulent flow in the ultimate regime. *Phys. Rev. Fluids* (submitted).
- MALKUS, M. V. R. 1954 The heat transport and spectrum of thermal turbulence. *Proc. R. Soc. Lond.* A **225**, 196–212.
- MITTAL, R. & IACCARINO, G. 2005 Immersed boundary methods. Annu. Rev. Fluid Mech. 37, 239–261.
- PAWAR, S. S. & ARAKERI, J. H. 2018 Two regimes of flux scaling in axially homogeneous turbulent convection in vertical tube. *Phys. Rev. Fluids* 1 (4), 042401(R).
- PESKIN, C. S. 2002 The immersed boundary method. Acta Numer. 11, 479-517.

- VAN DER POEL, E. P., OSTILLA-MÓNICO, R., DONNERS, J. & VERZICCO, R. 2015 A pencil distributed finite difference code for strongly turbulent wall-bounded flows. *Comput. Fluids* 116, 10–16.
- PRIESTLEY, C. H. B. 1954 Convection from a large horizontal surface. Aust. J. Phys. 7, 176-201.
- QIU, X. L., XIA, K.-Q. & TONG, P. 2005 Experimental study of velocity boundary layer near a rough conducting surface in turbulent natural convection. J. Turbul. 6, 1–13.
- ROCHE, P. E., CASTAING, B., CHABAUD, B. & HEBRAL, B. 2001 Observation of the 1/2 power law in Rayleigh-Bénard convection. *Phys. Rev.* E **63**, 045303.
- RODRIGUEZ-ITURBE, I., MARANI, M., RIGON, R. & RINALDO, A. 1994 Self-organized river basin landscapes: fractal and multifractal characteristics. *Water Resour. Res.* **30** (12), 3531–3539.
- RUSAOUËN, E., LIOT, O., CASTAING, B., SALORT, J. & CHILLÀ, F. 2018 Thermal transfer in Rayleigh-Bénard cell with smooth or rough boundaries. J. Fluid Mech. 837, 443-460.
- SALORT, J., LIOT, O., RUSAOUEN, E., SEYCHELLES, F., TISSERAND, J.-C., CREYSSELS, M., CASTAING, B. & CHILLÁ, F. 2014 Thermal boundary layer near roughnesses in turbulent Rayleigh-Bénard convection: flow structure and multistability. *Phys. Fluids* 26, 015112.
- SHEN, Y., TONG, P. & XIA, K.-Q. 1996 Turbulent convection over rough surfaces. *Phys. Rev. Lett.* **76**, 908–911.
- SHISHKINA, O. & WAGNER, C. 2011 Modelling the influence of wall roughness on heat transfer in thermal convection. J. Fluid Mech. 686, 568–582.
- SPIEGEL, E. A. 1963 A generalization of the mixing-length theory of turbulent convection. *Astrophys. J.* **138**, 216–225.
- STRINGANO, G. & VERZICCO, R. 2006 Mean flow structure in thermal convection in a cylindrical cell of aspect-ratio one half. J. Fluid Mech. 548, 1–16.
- TISSERAND, J. C., CREYSSELS, M., GASTEUIL, Y., PABIOU, H., GIBERT, M., CASTAING, B. & CHILLA, F. 2011 Comparison between rough and smooth plates within the same Rayleigh-Bénard cell. *Phys. Fluids* 23 (1), 015105.
- TOPPALADODDI, S., SUCCI, S. & WETTLAUFER, J. S. 2017 Roughness as a route to the ultimate regime of thermal convection. *Phys. Rev. Lett.* **118**, 074503.
- VERZICCO, R. & ORLANDI, P. 1996 A finite-difference scheme for three-dimensional incompressible flow in cylindrical coordinates. J. Comput. Phys. 123, 402–413.
- VILLERMAUX, E. 1998 Transfer at rough sheared interfaces. Phys. Rev. Lett. 81 (22), 4859-4862.
- WAGNER, S. & SHISHKINA, O. 2015 Heat flux enhancement by regular surface roughness in turbulent thermal convection. J. Fluid Mech. 763, 109–135.
- WEI, P., CHAN, T.-S., NI, R., ZHAO, X.-Z. & XIA, K.-Q. 2014 Heat transport properties of plates with smooth and rough surfaces in turbulent thermal convection. J. Fluid Mech. 740, 28–46.
- XIA, K.-Q. 2013 Current trends and future directions in turbulent thermal convection. Theor. Appl. Mech. Lett. 3 (5), 052001.
- XIE, Y.-C. & XIA, K.-Q. 2017 Turbulent thermal convection over rough plates with varying roughness geometries. J. Fluid Mech. 825, 573–599.
- YANG, X. I. A. & MENEVEAU, C. 2017 Modelling turbulent boundary layer flow over fractal-like multiscale terrain using large-eddy simulations and analytical tools. *Phil. Trans. R. Soc. Lond.* A 375 (2091), 20160098.
- ZHANG, Y.-Z., SUN, C., BAO, Y. & ZHOU, Q. 2018 How surface roughness reduces heat transport for small roughness heights in turbulent Rayleigh–Bénard convection. J. Fluid Mech. 836, R2.
- ZHU, X., MATHAI, V., STEVENS, R. J. A. M., VERZICCO, R. & LOHSE, D. 2018a Transition to the ultimate regime in two-dimensional Rayleigh–Bénard convection. *Phys. Rev. Lett.* **120** (14), 144502.
- ZHU, X., OSTILLA-MONICO, R., VERZICCO, R. & LOHSE, D. 2016 Direct numerical simulation of Taylor–Couette flow with grooved walls: torque scaling and flow structure. J. Fluid Mech. 794, 746–774.
- ZHU, X., PHILLIPS, E., SPANDAN, V., DONNERS, J., RUETSCH, G., ROMERO, J., OSTILLA-MÓNICO, R., YANG, Y., LOHSE, D., VERZICCO, R., MASSIMILIANO, F. & STEVENS, R. J. A. M. 2018b AFiD-GPU: a versatile Navier–Stokes solver for wall-bounded turbulent flows on GPU clusters. *Comput. Phys. Commun.* 229, 199–210.

869 R4-12

- ZHU, X., STEVENS, R. J. A. M., VERZICCO, R. & LOHSE, D. 2017 Roughness-facilitated local 1/2 scaling does not imply the onset of the ultimate regime of thermal convection. *Phys. Rev. Lett.* **119** (15), 154501.
- ZHU, X., VERSCHOOF, R. A., BAKHUIS, D., HUISMAN, S. G., VERZICCO, R., SUN, C. & LOHSE, D. 2018c Wall roughness induces asymptotic ultimate turbulence. *Nat. Phys.* 14 (4), 417–423.